## **Symbols**

Α	area, m <sup>2</sup>	Fo
$A_b$	area of prime (unfinned) surface, m <sup>2</sup>	Fr
$A_c$	cross-sectional area, m <sup>2</sup>	f
$A_p$	fin profile area, m <sup>2</sup>	G
Á <sub>r</sub>	nozzle area ratio	Gr
а	acceleration, m/s <sup>2</sup> ; speed of sound, m/s	Gz
Bi	Biot number	g
Bo	Bond number	H
С	molar concentration, kmol/m <sup>3</sup> ; heat capacity rate, W/K	h
$C_D$	drag coefficient	$h_{fg}$
$C_{f}$	friction coefficient	$h'_{fg}$
$\dot{C_t}$	thermal capacitance, J/K	$h_{sf}$
Со	Confinement number	$h_m$
С	specific heat, J/kg · K; speed of light, m/s	$h_{\rm rad}$
$C_p$	specific heat at constant pressure, J/kg · K	Ι
$c_v$	specific heat at constant volume, J/kg·K	i
D	diameter, m	
$D_{AB}$	binary mass diffusivity, m <sup>2</sup> /s	J
$D_b$	bubble diameter, m	Ja
$D_h$	hydraulic diameter, m	$J_i^*$
d	diameter of gas molecule, nm	
Ε	thermal plus mechanical energy, J; electric potential, V; emissive power, W/m <sup>2</sup>	$\dot{J}_i$
$E^{\text{tot}}$	total energy, J	$j_H$
Ec	Eckert number	$j_m$
$\dot{E}_{g}$ $\dot{E}_{in}$	rate of energy generation, W	k
$\dot{E}_{in}$	rate of energy transfer into a control volume, W	$k_B$
$\dot{E}_{out}$	rate of energy transfer out of control volume, W	$k_0$
$\dot{E}_{ m st}$	rate of increase of energy stored within a control volume, W	$k_1$
е	thermal internal energy per unit mass, J/kg;	
	surface roughness, m	$k_1''$
F	force, N; fraction of blackbody radiation in a	L
	wavelength band; view factor	Le

Fourier number
Froude number
friction factor; similarity variable
irradiation, W/m <sup>2</sup> ; mass velocity, kg/s · m <sup>2</sup>
Grashof number
Graetz number
gravitational acceleration, m/s <sup>2</sup>
nozzle height, m; Henry's constant, bars
convection heat transfer coefficient, $W/m^2 \cdot K$ ;
Planck's constant, J · s
latent heat of vaporization, J/kg
modified heat of vaporization, J/kg
latent heat of fusion, J/kg
convection mass transfer coefficient, m/s
radiation heat transfer coefficient, W/m <sup>2</sup> · K
electric current, A; radiation intensity, $W/m^2 \cdot sr$
electric current density, A/m <sup>2</sup> ; enthalpy per unit
mass, J/kg
radiosity, W/m <sup>2</sup>
Jakob number
diffusive molar flux of species <i>i</i> relative to the
mixture molar average velocity, kmol/s · m <sup>2</sup>
diffusive mass flux of species <i>i</i> relative to the
mixture mass average velocity, kg/s · m <sup>2</sup>
Colburn <i>j</i> factor for heat transfer
Colburn <i>j</i> factor for mass transfer
thermal conductivity, W/m · K
Boltzmann's constant, J/K
zero-order, homogeneous reaction rate
constant, kmol/s $\cdot$ m <sup>3</sup>
first-order, homogeneous reaction rate
constant, $s^{-1}$
first-order, surface reaction rate constant, m/s
length, m

Lewis number

М	mass, kg	$R_{t,o}$	thermal resistance of fin array, K/W
$\dot{M}_i$	rate of transfer of mass for species, <i>i</i> , kg/s	$r_o$	cylinder or sphere radius, m
$\dot{M}_{i,g}$	rate of increase of mass of species <i>i</i> due to	r, φ, z	cylindrical coordinates
<i>1,g</i>	chemical reactions, kg/s	r, θ, φ	spherical coordinates
$\dot{M}_{ m in}$	rate at which mass enters a control volume, kg/s	S	solubility, kmol/ $m^3 \cdot atm$ ; shape factor for
M <sub>m</sub> M <sub>out</sub>	rate at which mass leaves a control	5	two-dimensional conduction, m; nozzle
out	volume, kg/s		pitch, m; plate spacing, m; Seebeck
$\dot{M}_{\rm st}$	rate of increase of mass stored within a		coefficient, V/K
IVI st	control volume, kg/s	$S_c$	solar constant, W/m <sup>2</sup>
$\mathcal{M}_i$	molecular weight of species <i>i</i> , kg/kmol	$S_c$ $S_D, S_L, S_T$	diagonal, longitudinal, and transverse pitch
Ma	Mach number	$S_D, S_L, S_T$	of a tube bank, m
m	mass, kg	Sc	Schmidt number
m	mass, kg mass flow rate, kg/s	Sh	Sherwood number
$m_i$	mass flow rate, kg/s mass fraction of species $i$ , $\rho_i/\rho$	St	Stanton number
N N	integer number	T T	temperature, K
$N_L, N_T$	number of tubes in longitudinal and	t	time, s
$I_{V_L}, I_{V_T}$	transverse directions	U U	overall heat transfer coefficient, $W/m^2 \cdot K$ ;
Nu	Nusselt number	0	internal energy, J
NTU	number of transfer units	u, v, w	mass average fluid velocity components, m/s
	molar transfer rate of species <i>i</i> relative to	u, v, w u*, v*, w*	
N <sub>i</sub>	fixed coordinates, kmol/s	$U^{\circ}, U^{\circ}, W^{\circ}$ V	volume, m <sup>3</sup> ; fluid velocity, m/s
$N''_i$	molar flux of species <i>i</i> relative to fixed	v	specific volume, m <sup>3</sup> /kg
IVi	coordinates, kmol/s $\cdot$ m <sup>2</sup>	U W	width of a slot nozzle, m
$\dot{N}_i$	molar rate of increase of species <i>i</i> per unit	Ŵ	rate at which work is performed, W
IVi	volume due to chemical reactions,	w We	Weber number
	kmol/s $\cdot$ m <sup>3</sup>	X	vapor quality
$N_i''$	surface reaction rate of species <i>i</i> ,		Martinelli parameter
IVi	kmol/s $\cdot$ m <sup>2</sup>	$X_{tt}$ X, Y, Z	components of the body force per unit
$\mathcal{N}$	Avogadro's number	Λ, Ι, Ζ	volume, N/m <sup>3</sup>
$n_i''$	mass flux of species <i>i</i> relative to fixed	x, y, z	rectangular coordinates, m
n <sub>i</sub>	coordinates, kg/s $\cdot$ m <sup>2</sup>		critical location for transition to turbulence, m
$\dot{n}_i$	mass rate of increase of species <i>i</i> per unit	$x_c$	concentration entry length, m
n <sub>i</sub>	volume due to chemical reactions,	$x_{\mathrm{fd},c}$	hydrodynamic entry length, m
	kg/s $\cdot$ m <sup>3</sup>	$x_{\mathrm{fd},h}$	thermal entry length, m
Р	power, W; perimeter, m	$x_{\mathrm{fd},t}$ $x_i$	mole fraction of species $i, C_i/C$
$P_L, P_T$	dimensionless longitudinal and transverse	Z	thermoelectric material property, $K^{-1}$
1 L, 1 T	pitch of a tube bank	L	diemoeleette material property, K
Pe	Peclet number	Greek Lett	ers
Pr	Prandtl number	α	thermal diffusivity, m <sup>2</sup> /s; accommodation
p	pressure, N/m <sup>2</sup>	u	coefficient; absorptivity
$\overset{P}{Q}$	energy transfer, J	β	volumetric thermal expansion coefficient, $K^{-1}$
$\frac{\varphi}{q}$	heat transfer rate, W	Г	mass flow rate per unit width in film
$\dot{q}$	rate of energy generation per unit	•	condensation, kg/s · m
9	volume, W/m <sup>3</sup>	γ	ratio of specific heats
q'	heat transfer rate per unit length, W/m	δ	hydrodynamic boundary layer thickness, m
q''	heat flux, W/m <sup>2</sup>	$\delta_c$	concentration boundary layer thickness, m
$q^*$	dimensionless conduction heat rate	$\delta_p$	thermal penetration depth, m
R	cylinder radius, m; gas constant, J/kg·K	$\delta_t$	thermal boundary layer thickness, m
R	universal gas constant, J/kmol·K	ε	emissivity; porosity; heat exchanger
Ra	Rayleigh number		effectiveness
Re	Reynolds number	$\mathcal{E}_{f}$	fin effectiveness
R <sub>e</sub>	electric resistance, $\Omega$	η	thermodynamic efficiency; similarity variable
R <sub>f</sub>	fouling factor, $m^2 \cdot K/W$	$\eta_f$	fin efficiency
$R_m$	mass transfer resistance, s/m <sup>3</sup>	$\eta_o$	overall efficiency of fin array
$R_{m,n}$	residual for the <i>m</i> , <i>n</i> nodal point	$\theta$	zenith angle, rad; temperature difference, K
$R_{t}$	thermal resistance, K/W	ĸ	absorption coefficient, $m^{-1}$
$R_{t,c}$	thermal contact resistance, K/W	λ	wavelength, $\mu m$
$R_{t,f}$	fin thermal resistance, K/W	$\lambda_{ m mfp}$	mean free path length, nm
*:J		mp	

## Symbols

$\mu$	viscosity, kg/s · m	h	hydrodynamic; hot fluid; helical	
ν	kinematic viscosity, $m^2/s$ ; frequency of radiation, $s^{-1}$	i	general species designation; inner surface of an annulus; initial condition; tube inlet	
0	mass density, kg/m <sup>3</sup> ; reflectivity		condition; incident radiation	
ρ		L		
$\rho_e$	electric resistivity, $\Omega/m$	L 1	based on characteristic length	
$\sigma$	Stefan–Boltzmann constant, $W/m^2 \cdot K^4$ ; electrical		saturated liquid conditions	
	conductivity, $1/\Omega \cdot m$ ; normal viscous stress,	lat	latent energy	
A	$N/m^2$ ; surface tension, $N/m$	lm m	log mean condition	
Φ	viscous dissipation function, s <sup>-2</sup>		mean value over a tube cross section	
$\varphi$	volume fraction		maximum	
$\phi$	azimuthal angle, rad	0	center or midplane condition; tube outlet	
$\psi$	stream function, m <sup>2</sup> /s		condition; outer	
au	shear stress, N/m <sup>2</sup> ; transmissivity	р	momentum	
ω	solid angle, sr; perfusion rate, $s^{-1}$	ph	phonon	
		R	reradiating surface	
Subscri	pts	r, ref	reflected radiation	
A, B	species in a binary mixture	rad	radiation	
abs	absorbed	S	solar conditions	
am	arithmetic mean	S	surface conditions; solid properties;	
atm	atmospheric		saturated solid conditions	
b	base of an extended surface; blackbody	sat	saturated conditions	
С	carnot	sens	sensible energy	
с	cross-sectional; concentration; cold fluid; critical	sky	sky conditions	
cr	critical insulation thickness	SS	steady state	
cond	conduction	sur	surroundings	
conv	convection	t	thermal	
CF	counterflow	tr	transmitted	
D	diameter; drag	υ	saturated vapor conditions	
dif	diffusion	x	local conditions on a surface	
е	excess; emission; electron	λ	spectral	
evap	evaporation	~	free stream conditions	
f	fluid properties; fin conditions; saturated liquid			
5	conditions	Supersc	rscripts	
fc	forced convection	*	molar average; dimensionless quantity	
fd	fully developed conditions		•	
g	saturated vapor conditions	Overbar		
H	heat transfer conditions	-	surface average conditions; time mean	
			U ,	

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